

9. PID Controller

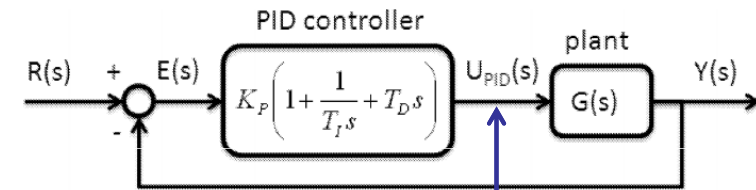
EN2142 Electronic Control Systems



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Three Term Controller

- Most popular industrial controller
- Can handle any industrial plant easily and satisfactorily
- Three gain controller $[K_P K_D K_I]$ or $[K_P T_D T_I]$
- **P**roportional, **D**erivative, and **I**ntegral control actions
- Weighted sum of three terms using gains



$$U_{PID}(s) = K_P e(s) + K_I \frac{E(s)}{s} + K_D s E(s)$$

$$U_{PID}(s) = K_P \left\{ E(s) + \frac{1}{T_I} \frac{E(s)}{s} + T_D s E(s) \right\} \quad \begin{matrix} T_i = \frac{K_P}{K_I} \\ T_d = \frac{K_D}{K_P} \end{matrix}$$

Proportional Term

- Determines the **responsiveness** of the controller
 - Aggressive/Weak
 - Increase/Decrease system bandwidth

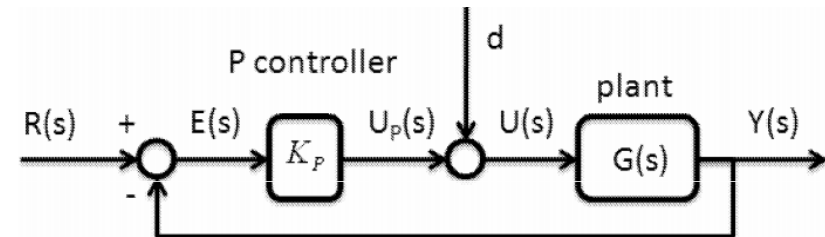
$$e(t) = r(t) - y(t)$$

- Positive command when $r(t) > y(t)$
- Negative command when $r(t) < y(t)$

- K_p is very BIG
 - Controller is sensitive
 - Responds to even small errors)
- K_p is very small
 - Controller is not sensitive
 - Respond only to BIG errors

Both extremes are not acceptable

Error due to Persistent Disturbances



- At equilibrium state

$$K_p e_{ss} + d = 0$$

$$e_{ss} = -\frac{d}{K_p}$$

P controller alone cannot eliminate the steady state error

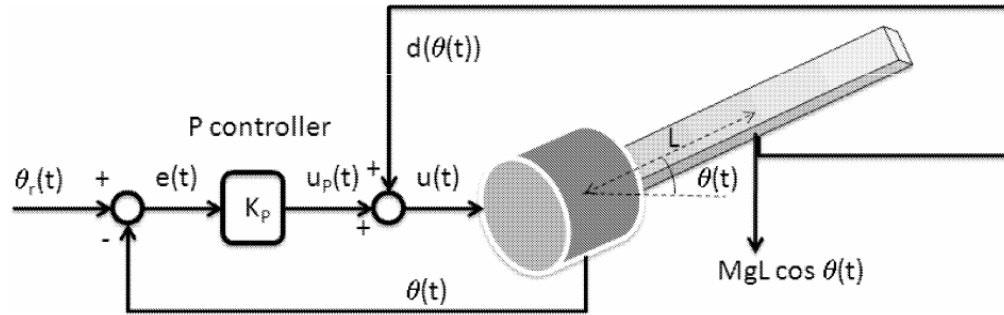
- Introduce an I-controller. Then, at equilibrium state

$$K_p e(t) + K_I \int e(t) dt + d = 0$$

$$e(t) = 0 \text{ and } \int e(t) dt = -d$$

Example

- Robot link position P-control system $K_p = 25, M = 3\text{kg}$
 $L = 1\text{m}, g = 9.8\text{ms}^{-2}$



P controller needs an error to generate torque to counter gravity, then reach steady state

$$K_p(\theta_r - \theta_{ss}) - MgL \cos \theta_{ss} = 0$$

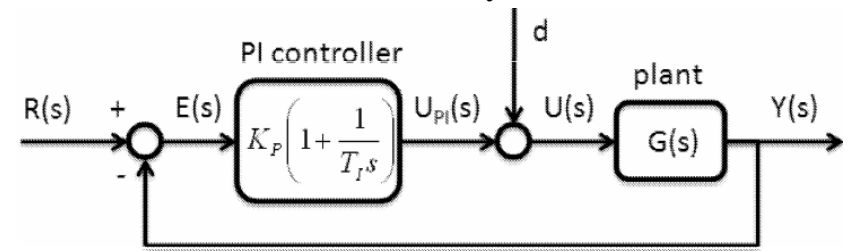
$$\theta_{ss} + \frac{MgL \cos \theta_{ss}}{K_p} - \theta_r = 0$$

$$\theta_{ss} + \frac{3 \times 9.8 \times 1 \cos \theta_{ss}}{25} - 1 = 0$$

$$\theta_{ss} = 0.15\text{rad} \quad \leftarrow \quad \theta_{ss} + 0.85 \cos \theta_{ss} - 1 = 0$$

I Controller

- Can eliminate steady state error
- If $y(t) < r(t)$ then $e(t) > 0 \quad u_I(t) = \int e(t)dt > 0$ drives $y(t) \rightarrow r(t)$



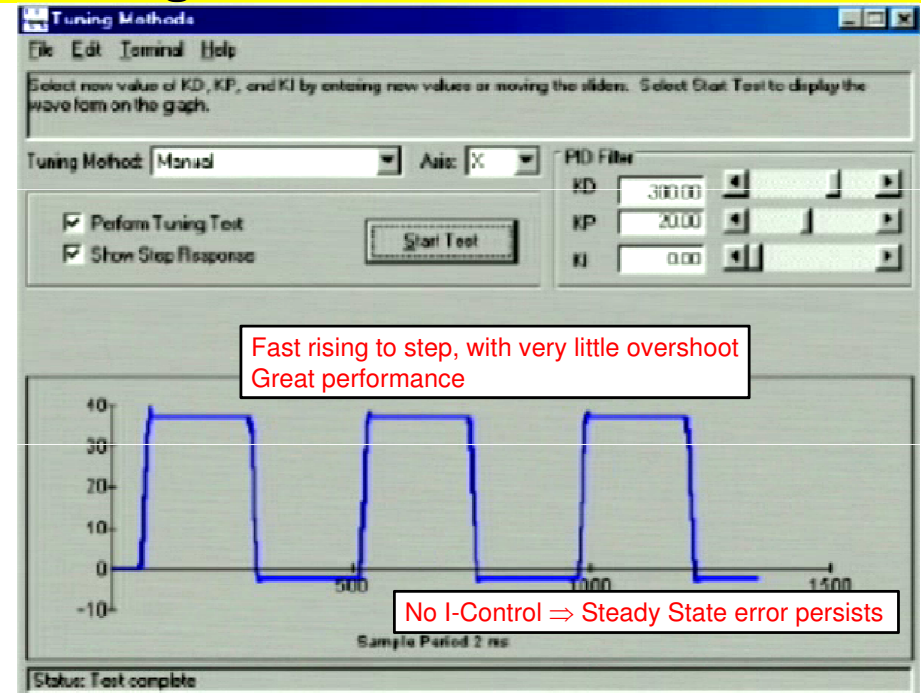
- Caution:** Error accumulation together, with a BIG value of K_I could generate large control commands causing response $y(t)$ to overshoot/undershoot (stability problem)
 - Reduce $K_I (= K_p / T_I)$ to reduce overshoot but it will take time to correct steady state errors

D - Controller

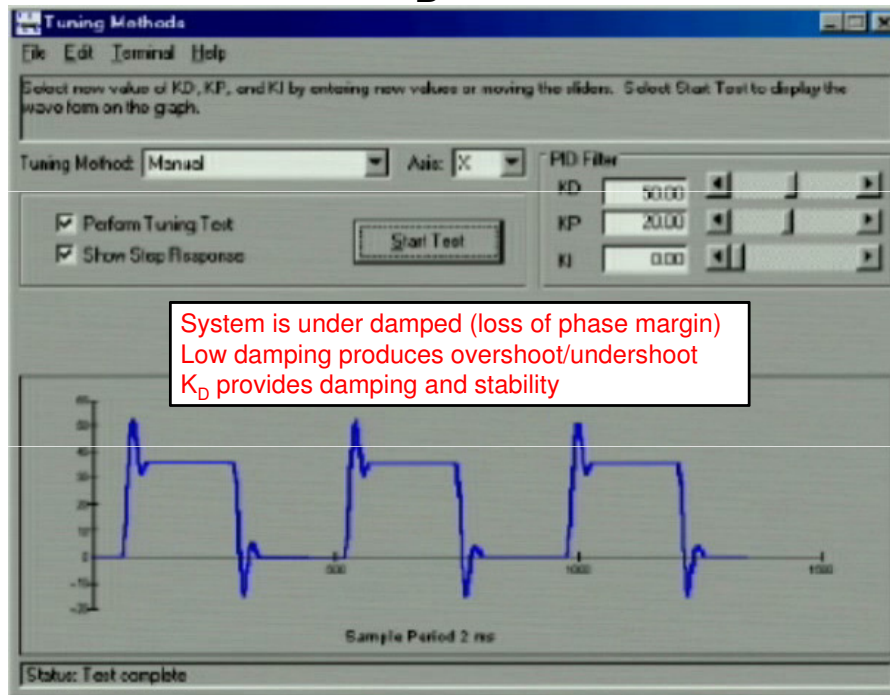
- Corrective action is proportional to the rate of change of error $\dot{e}(t) = \dot{r}(t) - \dot{y}(t)$
- For constant reference $\dot{r}(t) = 0$ and $u_D(t) = -K_D \dot{y}(t)$
- If a **negative error is dropping faster (unstable?)**, strong positive action is taken to stop and correct it
- If a **positive error is rising faster (unstable?)**, strong negative action is taken
- When the error doesn't change, no control action is taken (doesn't try to correct steady errors)

Improves Stability

Tuning PD Gains in Motion Control

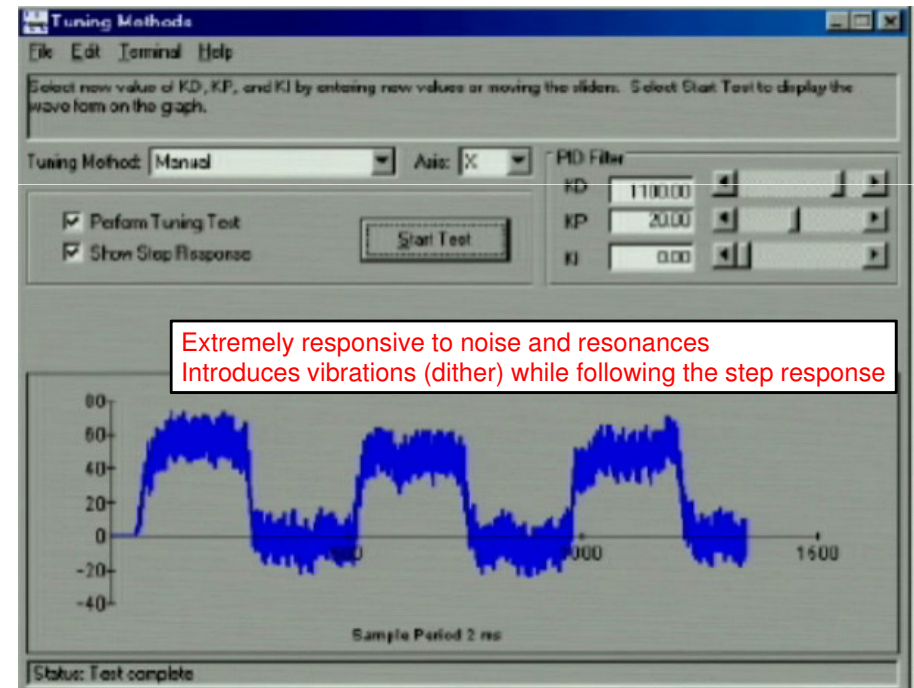


When K_D is too Low



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When K_D is too High



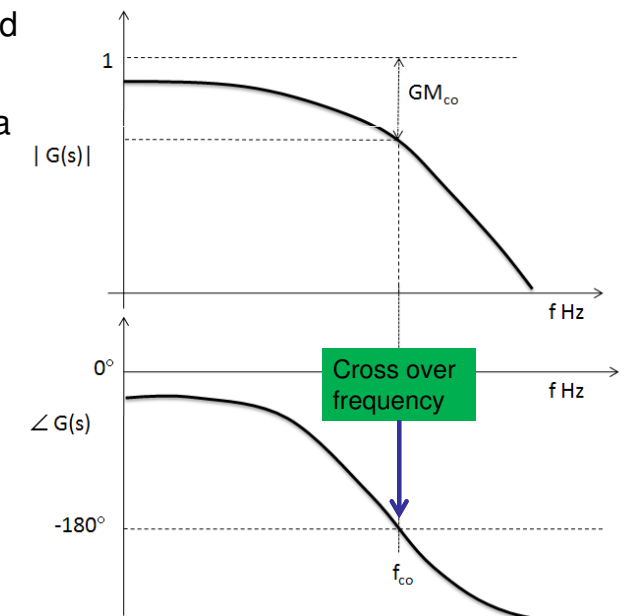
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Tuning PID Controller

- Best match between $[K_P K_D K_I]$ or $[K_P T_D T_I]$
- K_P makes the system responsive to errors, however, a bigger value of K_P will make the system too sensitive, and responsive to even noise in the control loop. K_I reduces the steady state error, however, it increases overshoot and reduces stability. K_D stabilizes the system by slowing down the response.
- In order to realize desirable response the three individual controllers have to be properly adjusted
- There are three main techniques for PID controller tuning
 - Zeigler-Nichols
 - Cohen-Coon
 - ITAE based methods

Ziegler-Nochols Method

- Frequency response of the plant is required
- Plant needs to have a crossover frequency f_{co} and stable gain margin Gm_{co}



Ziegler-Nichols Method

controller	K_P	K_I	K_D	T_I	T_D
P	$0.5GM$	-	-	-	-
PI	$0.45GM$	$1.2\frac{K_P}{T_{co}}$	-	$0.8T_{co}$	-
PID	$0.6GM$	$2\frac{K_P}{T_{co}}$	$0.125 K_P T_{co}$	$0.5 T_{co}$	$0.125 T_{co}$